

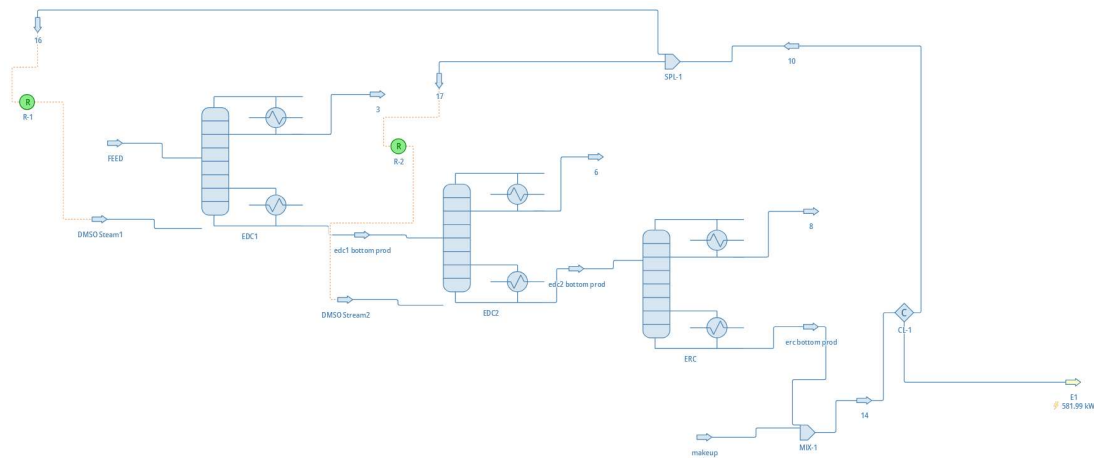
Energy-efficient recovery of tetrahydrofuran and ethyl acetate by triple-column extractive distillation: entrainer design and process optimization

Himisha Tapadiya
School of Chemical Engineering
B.Tech Chemical Engineering
Vellore Institute of Technology, Vellore

ABSTRACT

This work presents an energy-efficient process for recovering tetrahydrofuran (THF) and ethyl acetate (EtAC) from industrial effluent using a triple-column extractive distillation system. Thermodynamic analysis and Computer-Aided Molecular Design (CAMD) identified dimethyl sulfoxide (DMSO) as the optimal entrainer. The flowsheet employs a direct separation approach in which the feed stream, composed of water, EtAC, and THF, is introduced into the first extractive distillation column (EDC1) along with a pure DMSO stream. The distillate from EDC1 yields a high-purity THF product (99%), while the bottoms, containing DMSO, EtAC, water, and trace THF, are fed to the second extractive distillation column (EDC2). A supplementary DMSO stream enhances separation in EDC2, producing a 99% pure EtAC distillate and a bottoms stream consisting primarily of water and DMSO. The bottoms from EDC2 undergo further processing in an entrainer recovery column (ERC), where DMSO is separated from water. The ERC distillate is a purified water stream, while the bottoms consist of 99.99% pure DMSO. This recovered DMSO is cooled, combined with a makeup stream, and split into two recycle streams, which are reintroduced into EDC1 and EDC2 to optimize entrainer reuse. The process demonstrates efficient recovery of high-purity THF and EtAC from industrial wastewater, validating extractive distillation with DMSO as an effective separation method.

Flow Sheet



Result

Property / Streams	Units	10	14	16	17
Temperature	K	308.15	436.3375979	308.15	308.15
Pressure	bar	0.5	0.5	0.5	0.5
Molar Flow	kmol/h	103.6859 2	103.68592	75.01676312	28.66915688
Molar Fraction (Overall Liquid) / Ethyl acetate		0.000038 57804415	0.000037898 84308	0.000038578 04415	0.000038578 04415
Molar Fraction (Overall Liquid) / Dimethyl sulfoxide		0.999084 2856	0.999087175 1	0.999084285 6	0.999084285 6
Molar Fraction (Overall Liquid) / Tetrahydrofuran		0.000038 57804415	0.000037813 68936	0.000038578 04415	0.000038578 04415
Molar Fraction (Overall Liquid) / Water		0.000838 5583004	0.000837112 384	0.000838558 3004	0.000838558 3 004

Property / Streams	Units	3	6	8	DMSO Steam1	DMSO Stream2
Temperature	K	318.8397297	330.26288 31	354.37678 1	308.15	308.15
Pressure	bar	0.5	0.5	0.5	0.5	0.5
Molar Flow	kmol/h	32.98560312	33.040276 88	33.99012	75.016763 12	28.669156 88
Molar Fraction (Overall Liquid) / Ethyl acetate		0.0039959564 92	0.9948260 562	0.0000842 3492037	0.0000385 7804415	0.0000385 7804415
Molar Fraction (Overall Liquid) / Dimethyl sulfoxide		0	0.0000947 8633107	0.0005553 17854	0.9990842 856	0.9990842 856
Molar Fraction (Overall Liquid) / Tetrahydrofuran		0.9957061978	0.0048434 52758	0.0000000 44667796 26	0.0000385 7804415	0.0000385 7804415
Molar Fraction (Overall Liquid) / Water		0.0002978456 629	0.0002357 047216	0.9993604 026	0.0008385 583004	0.0008385 583004

Property / Streams	Units	edc1 bottom prod	edc2 bottom prod	erc bottom prod	FEED	makeup
Temperature	K	345.1285041	407.040380 6	436.463314 9	313.15	298.15
Pressure	bar	0.5	0.5	0.5	0.5	0.5
Molar Flow	kmol/h	142.03116	137.66004	103.66992	100	0.016
Molar Fraction (Overall Liquid) / Ethyl acetate		0.231435728 4	0.00002079 87349	0	0.33	0.25
Molar Fraction (Overall Liquid) / Dimethyl sulfoxide		0.527806453 3	0.75262108 69	0.99919989 63	0	0.25
Molar Fraction (Overall Liquid)		0.001118941 325	0.00000001 102907937	0	0.33	0.25

Liquid) / Tetrahydrofu ran						
Molar Fraction (Overall Liquid) / Water		0.239638877	0.24735810 34	0.00080010 3722	0.34	0.25

References

Yang, A., Su, Y., Shi, T., Ren, J., Shen, W., & Zhou, T. (2022). Energy-efficient recovery of tetrahydrofuran and ethyl acetate by triple-column extractive distillation: Entrainer design and process optimization. *Frontiers of Chemical Science and Engineering*, 16(2), 303–315.
<https://doi.org/10.1007/s11705-021-2044-z>