

# Production of Methyl Isobutyl Ketone from Acetone and Hydrogen

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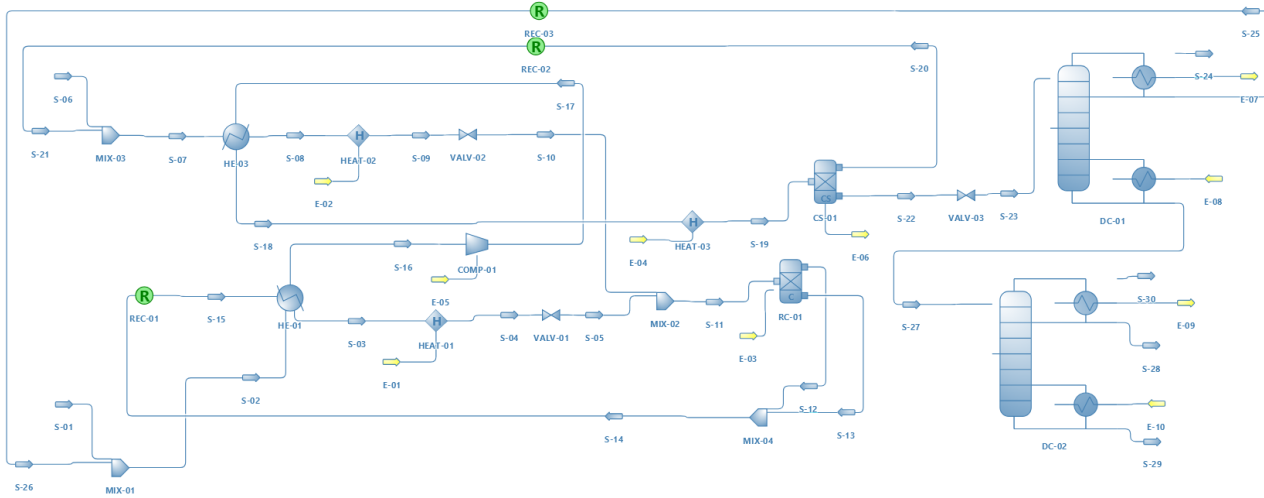
## Background:

Methyl Isobutyl Ketone (MIBK) can be produced by using low pressure one step gas phase process. Acetone and Hydrogen are used as a feed and nano-Pd/nano-ZnCr-O as a catalyst at about 1 atmospheric pressure. MIBK is generally used as a solvent for many industries. (1)

## Process description:

Pure Acetone feed (S-01) and recycled acetone (S-26) is mixed in mixer (MIX-01). The mixed acetone feed (S-02) enters the Heat exchanger (HE -01), where it exchanges the Heat associated with the reactor effluent. The outlet stream (S-03) enters the heater (HEAT-01) for further heating and then to pressure reducing valve (VALV-01) before entering to the mixture (MIX- 02) and the conversion reactor (RC-01). Simultaneously Pure hydrogen feed (S-06) and recycled hydrogen (S-21) is mixed in mixer (MIX-03) .The mixed hydrogen feed (S-07) enters the heat exchanger (HE-03) and then heater (HEAT-02) for further heating and then to pressure reducing valve (VALV-02).Now , the mixed acetone feed stream (S-05 ) and mixed hydrogen feed (S-10) enters the mixture (MIX-02) and then the mixture (S-11) enters the Conversion reactor (RC-01).Where the conversion reaction takes place in the vapor phase with the average acetone conversion being specified as 70 %.The conversion depends upon the catalyst and various other parameters, so an average conversion of 70 % is taken. The reactor effluent contains unreacted acetone, unreacted hydrogen, MIBK and by-product as water. The reactor effluent (S-12) and (S-13) is mixed and stream (S-14) is obtained . (S-14) is recycled using (REC-01) which passes through (HE-01), (COMP-01), (HE-03), (HEAT -03). Stream(S-19) enters the compound separator (CS-01), where pure hydrogen (S-20) is obtained and recycled (REC-02) and mixed with pure hydrogen feed (S-06). The bottom product from (CS-01) i.e., stream (S-22) enters the Distillation column (DC-01) from which acetone obtained from the distillate is recycled (REC-03). The bottom product from (DC-01) enters the second distillation column (DC-02) from which mainly water (S-28) is obtained as distillate and pure MIBK is obtained as bottom product (S-29).

**Flowsheet:**



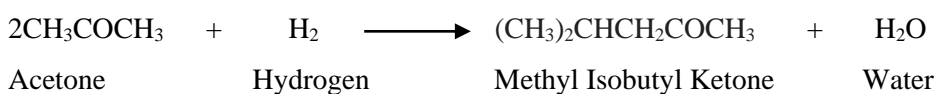
**Figure 1: One step synthesis of MIBK**

**Results:**

| Master Property Table                             |            |            |           |           |          |           |          |          |          |            |           |             |             |
|---|------------|------------|-----------|-----------|----------|-----------|----------|----------|----------|------------|-----------|-------------|-------------|
| Object  | S-01       | S-02       | S-03      | S-06      | S-07     | S-11      | S-14     | S-19     | S-20     | S-23       | S-25      | S-28        | S-29        |
| Temperature                                       | 343.15     | 338.912    | 623.15    | 298.15    | 302.761  | 622.709   | 788.354  | 308.15   | 308.15   | 308.15     | 338.994   | 377.066     | 385.544     |
| Pressure  | 182385     | 141855     | 141855    | 597818    | 349572   | 121590    | 120590   | 101325   | 101325   | 101325     | 101325    | 101325      | 101325      |
| Molar Flow  | 27.7778    | 60.3077    | 60.3077   | 14.0278   | 26.007   | 86.3147   | 72.4215  | 72.4215  | 12.1138  | 60.3077    | 35.1515   | 12.1562     | 13          |
| Volumetric Flow                                   | 0.00219969 | 0.00391242 | 2.20258   | 0.0581655 | 0.187268 | 3.67521   | 3.93629  | 0.385531 | 0.306291 | 0.00357447 | 0.0018625 | 0.000393228 | 0.00182738  |
| Molar Fraction (Mixture) / Hydrogen               | 0          | 0          | 0         | 1         | 1        | 0.301304  | 0.167268 | 0.167268 | 1        | 0          | 0         | 0           | 0           |
| Molar Fraction (Mixture) / Water                  | 0          | 0.25775    | 0.25775   | 0         | 0        | 0.180089  | 0.406475 | 0.406475 | 0        | 0.488122   | 0.49995   | 0.858957    | 0.000682531 |
| Molar Fraction (Mixture) / Acetone                | 1          | 0.658207   | 0.658207  | 0         | 0        | 0.459886  | 0.164433 | 0.164433 | 0        | 0.197462   | 0.338613  | 0.00128365  | 2.76814E-23 |
| Molar Fraction (Mixture) / Methyl isobutyl ketone | 0          | 0.0840431  | 0.0840431 | 0         | 0        | 0.0587205 | 0.261824 | 0.261824 | 0        | 0.314416   | 0.161437  | 0.139759    | 0.999317    |

**Conclusion and Recommendation:**

- A flowsheet for continuous production of MIBK was built with a product purity of 99% with the open-source Simulation tool DWSIM- Version 6.4.8 Classic UI.
- Since kinetic data related to catalytic single step reaction is not available in the open-source literature, we have used a conversion reactor model in the flowsheet with average acetone conversion of 70%.
- NRTL model was used a thermodynamical model and only a ' Single-Step reaction ' with no intermediate reaction and no intermediate product takes place as follow.



**References:**

1. Abdulrahman A. Al-Rabiah, Vagif Malik Akhmedov, Baku ,Abdulaziz A. Bagabas. *LOW PRESSURE ONE-STEP GAS-PHASE PROCESS FOR PRODUCTION OF METHYL ISOBUTYL KETONE*. s.l. : US 2011 023783, 2011.