## ABSTRACT FOR STOICHIOMETRIC REACTOR

## Description:

Stoichiometric reactor is used to get the composition of product stream given:

- Feed stream composition
- Coefficients of components involved in reaction
- Reaction Coordinate of each reaction

The important equations involved are:
$\mathrm{F}_{\mathrm{i}}=\mathrm{F}_{\mathrm{i} 0}-\left(\mathrm{v}_{\mathrm{i}} / \mathrm{v}_{\mathrm{A}}\right) \mathrm{X}_{\mathrm{A}} \mathrm{F}_{\mathrm{A} 0}$
$X_{A}=$ Amount of limiting reagent converted/Amount of limiting reagent present in mixture just before reaction
Where, $F_{i}$ is the molar flow rate of $\mathrm{i}^{\text {th }}$ component in product stream
$F_{i 0}$ is the molar flow rate of $\mathrm{i}^{\text {th }}$ component in feed stream
$v_{i}$ is the stoichiometry of $i^{\text {it }}$ component in reaction
$V_{A}$ is the stoichiometry of limiting reagent in reaction
$F_{A 0}$ is the molar flow rate of limiting reagent in feed stream
Product compositions of reactions are calculated using sequential method and not simultaneously i.e. the code solves for the product composition after first reaction, and then uses this updated composition to find the product composition of next reaction.
Limiting Reagent is found by calculating the molar composition/stoichiometry ratio for reactants of a particular reaction. The reagent with least ratio is the limiting reagent.

## References: http://www.iitg.ac.in/tamalb/documents/reactors.pdf

## Examples:

1)Component System: $\mathrm{CH}_{3} \mathrm{CHO}, \mathrm{CO}, \mathrm{CH}_{4}, \mathrm{O}_{2}, \mathrm{CO}_{2}$

Thermodynamic Package: Peng Robinson/Lee Kesler
Reaction: $\mathrm{CH}_{3} \mathrm{CHO} \rightarrow \mathrm{CO}+\mathrm{CH}_{4}$ (Fractional conversion $=0.3$ )
$1 / 2 \mathrm{O}_{2}+\mathrm{CO} \rightarrow \mathrm{CO}_{2}$ (Fractional conversion $=0.7$ )
Feed Composition: 0.5 moles $\mathrm{O}_{2}$ and 0.5 moles $\mathrm{CH}_{3} \mathrm{CHO}$

| Component | Method of Solving for number of moles |  |
| :---: | :---: | :---: |
|  | Analytical | DWSIM |
| $\mathrm{CH}_{3} \mathrm{CHO}$ | 0.35 | 0.34976363 |
| CO | 0.045 | 0.04496961 |
| $\mathrm{CH}_{4}$ | 0.15 | 0.1498987 |
| $\mathrm{O}_{2}$ | 0.4475 | 0.44719779 |
| $\mathrm{CO}_{2}$ | 0.105 | 0.10492909 |

2)Component System: $\mathrm{CH}_{3} \mathrm{CHO}, \mathrm{CO}, \mathrm{CH}_{4}, \mathrm{O}_{2}, \mathrm{CO}_{2}$ Thermodynamic Package: Soave-Redlich-Kwong (SRK)
Reaction: $\mathrm{CH}_{3} \mathrm{CHO} \rightarrow \mathrm{CO}+\mathrm{CH}_{4}$ (Fractional conversion $=0.3$ )
$1 / 2 \mathrm{O}_{2}+\mathrm{CO} \rightarrow \mathrm{CO}_{2}$ (Fractional conversion $=0.7$ )

Feed Composition: 0.1 moles $\mathrm{O}_{2}$ and 0.9 moles $\mathrm{CH}_{3} \mathrm{CHO}$

| Component | Method of Solving for number of moles |  |
| :---: | :---: | :---: |
|  | Analytical | DWSIM |
| $\mathrm{CH}_{3} \mathrm{CHO}$ | 0.63 | 0.62930623 |
| CO | 0.13 | 0.12985684 |
| $\mathrm{CH}_{4}$ | 0.27 | 0.26970267 |
| $\mathrm{O}_{2}$ | 0.03 | 0.029966964 |
| $\mathrm{CO}_{2}$ | 0.14 | 0.13984583 |

3) Component System: $\mathrm{C}_{2} \mathrm{H}_{6}, \mathrm{C}_{2} \mathrm{H}_{4}, \mathrm{H}_{2}, \mathrm{C}_{2} \mathrm{H}_{2}$

Thermodynamic Package: Soave-Redlich-Kwong (SRK)
Reaction: $\mathrm{C}_{2} \mathrm{H}_{6} \rightarrow \mathrm{C}_{2} \mathrm{H}_{4}+\mathrm{H}_{2}($ Fractional conversion $=0.5)$
$\mathrm{C}_{2} \mathrm{H}_{6} \rightarrow \mathrm{C}_{2} \mathrm{H}_{2}+2 \mathrm{H}_{2}($ Fractional conversion $=0.7)$
$\mathrm{C}_{2} \mathrm{H}_{4} \rightarrow \mathrm{C}_{2} \mathrm{H}_{2}+\mathrm{H}_{2}($ Fractional conversion $=0.8)$
Feed Composition: 0.6 moles $\mathrm{C}_{2} \mathrm{H}_{6}, 0.5$ moles $\mathrm{H}_{2}$ and 0.9 moles $\mathrm{C}_{2} \mathrm{H}_{4}$

| Component | Method of Solving for number of moles |  |
| :---: | :---: | :---: |
|  | Analytical | DWSIM |
| $\mathrm{C}_{2} \mathrm{H}_{6}$ | 0.09 | 0.0898025 |
| $\mathrm{C}_{2} \mathrm{H}_{4}$ | 0.24 | 0.23947333 |
| $\mathrm{C}_{2} \mathrm{H}_{2}$ | 1.17 | 1.1674325 |
| $\mathrm{H}_{2}$ | 1.22 | 2.1752161 |

4) Component System: $\mathrm{C}_{2} \mathrm{H}_{6}, \mathrm{C}_{2} \mathrm{H}_{4}, \mathrm{H}_{2}, \mathrm{C}_{2} \mathrm{H}_{2}$

Thermodynamic Package: UNIFAC
Reaction: $\mathrm{C}_{2} \mathrm{H}_{6} \rightarrow \mathrm{C}_{2} \mathrm{H}_{4}+\mathrm{H}_{2}($ Fractional conversion $=0.3)$
$\mathrm{C}_{2} \mathrm{H}_{6} \rightarrow \mathrm{C}_{2} \mathrm{H}_{2}+2 \mathrm{H}_{2}($ Fractional conversion $=0.2)$
$\mathrm{C}_{2} \mathrm{H}_{4} \rightarrow \mathrm{C}_{2} \mathrm{H}_{2}+\mathrm{H}_{2}($ Fractional conversion $=0.6)$
Feed Composition: 0.4 moles $\mathrm{C}_{2} \mathrm{H}_{6}, 0.9$ moles $\mathrm{H}_{2}$ and 0.1 moles $\mathrm{C}_{2} \mathrm{H}_{4}$

| Component | Method of Solving for number of moles |  |
| :---: | :---: | :---: |
|  | Analytical | DWSIM |
| $\mathrm{C}_{2} \mathrm{H}_{6}$ | 0.224 | 0.22336457 |
| $\mathrm{C}_{2} \mathrm{H}_{4}$ | 0.088 | 0.087750366 |
| $\mathrm{C}_{2} \mathrm{H}_{2}$ | 0.188 | 0.18746669 |
| $\mathrm{H}_{2}$ | 1.254 | 1.2604143 |

